

This Page Is Inserted by IFW Operations
and is not a part of the Official Record

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images may include (but are not limited to):

- BLACK BORDERS
- TEXT CUT OFF AT TOP, BOTTOM OR SIDES
- FADED TEXT
- ILLEGIBLE TEXT
- SKEWED/SLANTED IMAGES
- COLORED PHOTOS
- BLACK OR VERY BLACK AND WHITE DARK PHOTOS
- GRAY SCALE DOCUMENTS

IMAGES ARE BEST AVAILABLE COPY.

**As rescanning documents *will not* correct images,
please do not report the images to the
Image Problem Mailbox.**

THIS PAGE BLANK (USPTO)

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau

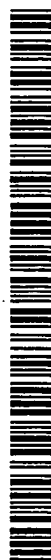


(43) International Publication Date
10 May 2001 (10.05.2001)

PCT

(10) International Publication Number
WO 01/32735 A1

- (51) International Patent Classification⁷: C08G 18/48, 18/10
- (21) International Application Number: PCT/EP00/09731
- (22) International Filing Date: 5 October 2000 (05.10.2000)
- (25) Filing Language: English
- (26) Publication Language: English
- (30) Priority Data:
99121697.9 2 November 1999 (02.11.1999) EP
- (71) Applicant (for all designated States except US): HUNTS-
MAN INTERNATIONAL LLC [US/US]; 500 Huntsman
Way, Salt Lake City, UT 84108 (US).
- (72) Inventors; and
- (75) Inventors/Applicants (for US only): PARFONDRY,
Alain [FR/BE]; Rue Longue 82, B-1150 Brussels (BE).
YU, Jianming [CN/BE]; Avenue Charles Woeste 66,
B-1090 Brussels (BE).
- (74) Agents: BAKEN, Philippus, Johannes, Leonardus,
Henricus et al.; Huntsman ICI (Europe) BVBA, Hunts-
man Polyurethanes, Intellectual Property Department,
Everslaan 45, B-3078 Everberg (BE).
- (81) Designated States (national): AE, AG, AL, AM, AT, AU,
AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CR, CU, CZ,
DE, DK, DM, DZ, EE, ES, FI, GB, GD, GE, GH, GM, HR,
HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR,
LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ,
NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM,
TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW.
- (84) Designated States (regional): ARIPO patent (GH, GM,
KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian
patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European
patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE,
IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG,
CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).
- Published:
— With international search report.
- For two-letter codes and other abbreviations, refer to the "Guid-
ance Notes on Codes and Abbreviations" appearing at the begin-
ning of each regular issue of the PCT Gazette.



WO 01/32735 A1

(54) Title: PROCESS FOR MAKING HIGH RESILIENCE FOAMS

(57) Abstract: The invention relates to a prepolymer process for preparing a high resilience flexible polyurethane foam by reacting a polyisocyanate composition comprising at least 80 % by weight of 4,4'-MDI and having an NCO value below 20 % with a polyol composition comprising b1) an EO-rich polyol; b2) a polyol with an EO content between 20-50 % and a primary hydroxy content of at least 50 %; and b3) a polyol with an EO content between 10-20 % and a primary hydroxy content of at least 50 %; according to the following proportions: b1 : 40-90 wt %, b2 : 5-60 wt %, b3 : 0-20 wt %. The invention also relates to reaction systems comprising the above components.

PROCESS FOR MAKING HIGH RESILIENCE FOAMS

The instant invention relates to a process for making high resilience foams, and to reaction systems that are useful in the said process.

EP-A-0547765 to Bleys et al. discloses a process for making high resilience foams comprising reacting high 4,4' MDI with an EO-rich polyol. While the foams thus obtained exhibit good properties, the process suffers from two main drawbacks. The first drawback is that this process, if to be used on large scale, necessarily makes use of a full prepolymer having a very high viscosity, rendering it difficult to process. Lowering the level of prepolymerization lead to foams that tend to close. The second drawback is that this process is very sensitive to the presence of a polyol that has an EO content (generally as tipped) from 10 to 20 % by weight. This polyol happens to be used in almost all kinds of foams and thus the equipment will always contain some of this polyol. Carrying out the process of this patent thus requires to clean the equipment very thoroughly before use.

US-P-5594097 to Chaffanjon discloses specific polyols, having the structure PO-PO/EO-EO. One example makes use of a mixture of this polyol with an EO-rich polyol; the resulting foam is said to be of poor quality.

WO 94/24183 discloses the preparation of flexible polyurethane foams using a polyisocyanate containing at least 85% by weight of 4,4'-MDI and a polyol composition comprising 25 to less than 50% by weight of oxyethylene groups; prepolymers may be used as well. Only up to 50% by weight of other polyols may be used.

US-P-5677361 to Treboux et al. discloses a process for making high resilience foams comprising reacting an isocyanate with a specific polyol composition, which comprises an EO-rich polyol, a classical polyol

comprising tipped EO, and a polymer polyol. This process however uses the EO-rich polyol in minor amounts.

The instant invention aims at solving these problems and at providing a process which is not sensitive to PO-rich polyols (EO contents below 20%) and which is easy to carry out, and at providing reaction systems which are easily processable. The instant invention also aims at providing foams with high resilience and low compression set values, low hysteresis loss (lower than 20%), and with latex-like feel.

The invention thus provides a prepolymer process for preparing a high resilience flexible polyurethane foam at an NCO index of 70-120, preferably 70-110, by reacting:

a) a polyisocyanate composition comprising at least 80% by weight of 4,4'-MDI;

b1) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxy functionality of 2-6, where the EO is present as tipped EO and/or random EO, the total EO content being at least 50 % by weight;

b2) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxy functionality of 2-6, where the EO is present as tipped EO and/or random EO, the total EO content being between 20-50 % by weight, having a primary hydroxy content of at least 50%;

b3) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxyl functionality of 2-6, having a primary hydroxy content of at least 50%, and having an EO content of from 10 to 20 % by weight;

these polyols b1, b2 and b3 being reacted according to the following proportions, based on the combined weights of b1, b2 and b3, b1 : 40-90 wt %, b2 : 5-60 wt %, b3 : 0-20 wt %;

c) water; and

d) additives and auxiliaries known per se;

and where the polyisocyanate prepolymer has an NCO value below 20% by weight.

The invention also relates to a reaction system comprising A) a polyisocyanate prepolymer obtained by reacting the polyisocyanate with part of the polyol composition of the invention, and B) an isocyanate-reactive component comprising the remainder of the polyol composition of the invention and water.

In the context of the present invention the following terms, if and whenever they are used, have the following meaning :

- 1) isocyanate index or NCO index :
the ratio of NCO-groups over isocyanate-reactive hydrogen atoms present in a formulation, given as a percentage :

$$\frac{[\text{NCO}] \times 100}{[\text{active hydrogen}]} \quad (\%)$$

In other words the NCO-index expresses the percentage of isocyanate actually used in a formulation with respect to the amount of isocyanate theoretically required for reacting with the amount of isocyanate-reactive hydrogen used in a formulation.

It should be observed that the isocyanate index as used herein is considered from the point of view of the actual foaming process involving the isocyanate ingredient and the isocyanate-reactive ingredients. Any isocyanate groups consumed in a preliminary step to produce modified polyisocyanates (including such isocyanate-derivatives referred to in the art as quasi or semi-prepolymers and prepolymers) or any active hydrogens reacted with isocyanate to produce modified polyols or polyamines, are not taken into account in the calculation of the isocyanate index. Only the free isocyanate groups and the free isocyanate-reactive hydrogens (including those of the water) present at the actual foaming stage are taken into account.

- 2) The expression "isocyanate-reactive hydrogen atoms" as used herein for the purpose of calculating the

isocyanate index refers to the total of hydroxyl and amine hydrogen atoms present in the reactive compositions in the form of polyols, polyamines and/or water; this means that for the purpose of calculating the isocyanate index at the actual foaming process one hydroxyl group is considered to comprise one reactive hydrogen, one primary or secondary amine group is considered to comprise one reactive hydrogen and one water molecule is considered to comprise two active hydrogens.

3) Reaction system : a combination of components wherein the polyisocyanate component is kept in a container separate from the isocyanate-reactive components.

4) The expression "polyurethane foam" as used herein generally refers to cellular products as obtained by reacting polyisocyanates with isocyanate-reactive hydrogen containing compounds, using foaming agents, and in particular includes cellular products obtained with water as reactive foaming agent (involving a reaction of water with isocyanate groups yielding urea linkages and carbon dioxide and producing polyurea-urethane foams).

5) The term "average nominal hydroxyl functionality" is used herein to indicate the average functionality (number of hydroxyl groups per molecule) of the polyol composition on the assumption that this is the average functionality (number of active hydrogen atoms per molecule) of the initiator(s) used in their preparation although in practice it will often be somewhat less because of some terminal unsaturation. The average equivalent weight of a polyol is the average molecular weight divided by this average nominal hydroxyl functionality.

6) The term "average" is used to indicate an average by number.

7) The term "high resilience foams" are intended to designate those foams having a resilience of

at least 40%, as measured according to ISO 8307.

The following way of describing polyols is used in the present application : A PO-EO polyol is a polyol having first a PO block attached to the initiator followed by an EO block. A PO-PO/EO polyol is a polyol having first a PO block and then a block of randomly distributed PO and EO. A PO-PO/EO-EO polyol is a polyol having first a PO block then a block of randomly distributed PO and EO and then a block of EO. A PO-EO polyol is a polyol having first a PO block and then an EO block. In the above descriptions only one tail of a polyol is described (seen from the initiator); the nominal hydroxy functionality will determine how many of such tails will be present.

The polyisocyanate used in the prepolymer comprises at least 80% by weight of 4,4'-MDI (methylene diphenyl isocyanate).

The remaining part may comprise isomers thereof, higher functionalities oligomers thereof, variants thereof, or any other isocyanate (such as TDI). The isomers can be 2,4'-MDI and/or 2,2'-MDI. The oligomers are known, like e.g. polymeric MDI having isocyanate functionalities above 2. Variants thereof are known variants containing carbodiimide, uretonimine, isocyanurate, urethane, allophanate, urea and/or biuret groups. Most preferred isocyanates are pure 4,4'-MDI (isomer content less than 4% by weight), mixtures of 4,4'-MDI with polymeric MDI, mixtures of 4,4'-MDI with uretonimine and/or carbodiimide and/or urethane modified MDI.

The polyisocyanate may contain dispersed urea particles and/or urethane particles prepared in a conventional way, e.g. by adding a minor amount of an amine such as isophorone diamine to the polyisocyanate.

The prepolymer is obtained by standard methods known to the skilled man. The NCO value is below 20% by weight (the value of 20% by weight is excluded), for example from 7 to 20% by weight, preferably below 15% by weight. Preferred range is 7 to 15% by weight.

Polyol b1 is an EO rich polyol. It can be prepared by known methods. It comprises PO and EO, where the EO can be random, tipped, or both. Preferably the EO is random in majority. The EO content is greater than 50% by weight (over the total oxyalkylene units present).

Polyol b2 may have a structure of the type PO-PO/EO-EO or of the type PO/EO-EO or of the type PO-EO. The total EO content is from 20 to 50 % by weight (over the total oxyalkylene units present), preferably from 21 to 45 %. Polyol b2 has a primary OH content of at least 50%, preferably at least 70% based on the primary and secondary hydroxyl groups in the polyol. In the PO-PO/EO-EO type polyol, the first PO block comprises preferably from 20 to 75 % by weight of the PO units. In those polyols b2) comprising both tipped and random EO, the weight ratio tipped EO/random EO preferably is from 1:3 to 3:1. The polyol having a structure of the type PO-PO/EO-EO can notably be produced according to the teaching of the Chaffanjon et al. US-A-5594097. The polyol having a structure of the type -PO/EO-EO can notably be produced according to the teaching of the Hostettler US-A-4559366. One example of a polyol b2) is one where the tipped EO content is from 10-20 % by weight.

Polyol b3 is an optional polyol. It can be prepared by known methods. It has a primary hydroxy content of at least 50%, preferably at least 70%. It can be of various structures (PO-EO, PO/EO, etc.), where the EO can be either random, tipped, or both. The EO content is from 10 to 20 % by weight (over the total oxyalkylene units present). A preferred polyol is one where EO is present as tipped EO.

The nominal functionality of these polyols b1, b2 and b3 is comprised between 2 and 6, preferably between 2 and 4.

5 The average equivalent weight of these polyols b1, b2 and b3 is generally comprised between 1000 and 4000, preferably 1500 and 3500.

The polyols are caused to react in the process according to the following proportions, expressed on the basis of the combined weights of the polyols:

10 b1 : 40-90 %, preferably 50-80 % by weight
b2 : 5-60 %, preferably 10-40 % by weight
b3 : 0-20 %, preferably 0-10% by weight.

Each component b1, b2 and b3 may be comprised of mixtures.

15 Dispersed material can also be present. This is known as polymer-modified polyol, and comprise e.g. SAN or PIPA (Poly Isocyanate Poly Addition), or PHD (polyurea suspension).

20 The polymer-modified polyols which are particularly interesting in accordance with the invention are products obtained by in situ polymerization of styrene and/or acrylonitrile in poly(oxyethylene/oxypropylene)polyols and products obtained by in situ reaction between a polyisocyanate and an amino- or hydroxy-functional
25 compound (such as triethanolamine) in a poly(oxyethylene/oxypropylene)polyol. The solids content (based on the total polyol weight b1+b2+b3) can vary within broad limits, e.g. from 5 to 50 %. Particle sizes of the dispersed polymer of less than 50 microns are preferred.
30 Mixtures can be used as well.

Water is used as the blowing agent. Carbon dioxide may be added if needed. It is appropriate to use from 1.0 to 15 %, preferably from 2 to 6 %, by weight of water based on the weight of the total polyol component
35 (prereacted and not prereacted, i.e. the total starting polyol or total starting isocyanate-reactive compounds),

where the water can optionally be used in conjunction with carbon dioxide.

Other conventional ingredients (additives and/or auxiliaries) may be used in making the polyurethanes. These include catalysts, for example, tertiary amines and organic tin compounds, surfactants, cross linking or chain extending agents, for example, low molecular weight compounds such as diols, triols (having a molecular weight below the one of b3) and diamines, flame proofing agents, for example, halogenated alkyl phosphates, fillers and pigments. Foam stabilizers, for example polysiloxane-polyalkylene oxide block copolymers, may be used to stabilize or regulate the cells of the foam.

The amount of these minor ingredients used will depend on the nature of the product required and may be varied within limits well known to a polyurethane foam technologist.

These components, notably the polyols b1, b2 and b3 can be added in any order, provided a prepolymer is used according to the NCO values indicated above. The polyols can be added one after the other, or part by part, in any order (for example, part of b1, then the remainder of b1 together with the all of b2+b3 or all of b2 then all of b1 then all of b3).

In one embodiment, the prepolymer is obtained with all the polyol b1, and no polyol b2 and b3, which are thus added in the resin side.

The components of the polyurethane forming reaction mixture may be mixed together in any convenient manner, for example the individual components may be pre-blended so as to reduce the number of component streams requiring to be brought together in the final mixing step. It is often convenient to have a two-stream system whereby one stream comprises the polyisocyanate prepolymer and the second stream comprises all the other components of the reaction mixture.

5 The flexible foams may be made according to the moulding or the slabstock technique. The foams may be preferably prepared by known moulding processes, hot or cold. The foams may be used in the furniture and automotive industries in seating, cushioning and
mattresses.

10 The flexible foams thus obtained have a free rise density comprised between, e.g. 30 and 80 kg/m³, preferably 35 and 65 kg/m³. These foams show a resilience higher than about 45 %, preferably higher than about 50 %.

15 The invention also provides a reaction system that will enable the foam producer to make the desired foam by reacting the polyisocyanate and polyol compositions. This approach provides a relatively simple way to the customer to make a product from often a variety of chemicals by combining two compositions under appropriate conditions. The polyisocyanate component is the prepolymer, while the isocyanate-reactive component comprises the remainder of
20 the polyol. Under this embodiment, any combination is foreseen. It covers notably the following possibilities: Part of b1+b2+b3 in the prepolymer, then the remainder of b1+b2+b3 in the isocyanate-reactive component; Part of b1+b2 but no b3, then the remainder of b1+b2 and all b3; 25 Part of b1+b3 but no b2, then the remainder of b1+b3 and all b2; all of b1, then the all of b2+b3; all of b2, then the all of b1+b3; Part of b1, then the remainder of b1 together with the all of b2+b3; Part of b2, then the remainder of b2 together with the all of b1+b3. In one
30 embodiment, the reaction system comprises A) a prepolymer obtained with all the b1 polyol and B) the remainder of the polyol and the other reactants.

The following examples illustrate the invention without limiting it.

35 Unless otherwise indicated, all parts are given by weight.

Glossary.

(all functionalities are nominal functionalities)

- Polyol A PO/EO, with EO as random. EO content is 75 % by weight. Average equivalent weight is 1336. Functionality is 3, OH value is 42 mg KOH/g.
- Polyol B PO-PO/EO-EO, total EO content is 28,6 % by weight. Tip EO content is 15 % by weight. Average equivalent weight is 2004. Functionality is 3, OH value is 28 mg KOH/g. Primary OH content is 87%.
- Polyol C PO-PO/EO-EO, total EO content is 21 % by weight. Tip EO content is 15 % by weight. Average equivalent weight is 2004. Functionality is 3, OH value is 28 mg KOH/g. Primary OH content is 83%.
- Polyol D PO/EO-EO, total EO content is 29.6 % by weight. Tip EO content is 15 % by weight. Average equivalent weight is 2004. Functionality is 3, OH value is 28 mg KOH/g. Primary OH content is 84%.
- Polyol E PO-EO, with EO as tipped. EO content is 15 % by weight. Average equivalent weight is 2004. Functionality is 3, OH value is 28 mg KOH/g. Primary OH content is 81%.
- Polyol F Polymer polyol, with 20% by weight of dispersed urethane solids from triethanolamine and uretonimine modified MDI in polyol E.
- Polyol G PEG having an average equivalent weight of 442. Functionality is 3.
- Isocyanate A Prepolymer based on pure 4,4'-MDI (functionality is 2) and polyol A. Functionality is 2.13. NCO value is 7.9% by weight.
- Isocyanate B Modified MDI comprising 72.8% by weight of MDI (2.0 % of which is 2,4'- and 2,2') and

27.2% by weight uretonimine-modified MDI.
 Functionality is 2.12. NCO value is 29.3%
 by weight.

B4113	Surfactant from Goldschmidt
Niax A1	Catalyst from Union Carbide
D33LV	Catalyst from Air Products

Foams are produced according to the following scheme.
 Polyols, catalysts, surfactant and water are mixed prior
 to the addition of isocyanates. Polyol blends and
 5 isocyanates are mixed at 20°C during 8 seconds before
 foaming. Free-rise foams are made in plastic buckets of
 2.5 l to 10 l.

The properties of the foam are determined according
 to the following methods and standards :

10	Nature of cells :	
	Recession (%)	
	FRD (Free Rise Density)	ISO 845
	Foaming	
	Cream Time (s)	
15	End Of Rise (s)	
	Compression hardness	
	CLD 40% (kPa)	ISO 3386-1
	Hysteresis Loss (%)	
	Compression set (thickness)	ISO 1856
20	Dry 75 % (%)	
	Humid 75 % (%)	
	Resilience (%)	ISO 8307
	Tear strength (N/m)	ISO 8067
	Max	
25	Tensile strength(kPa)	ISO 1798
	Elongation (%)	

The results are summarized in the following tables.

Component	Examples											
	1	2	3	4	5	6	7	8	9	10	11	12
Polyol A								6	11			
Polyol B	40	32	35	40		35	30	17	12		23	35
Polyol C					70							
Polyol D										35		
Polyol E							5					
Polyol F		10										
Polyol G			5									
Water	3	2.6	3	4	3.3	2.5	2.5	2.2	2.2	2.5	2.2	2.5
B 4113		1	0.5	0.5		0.5	0.5	0.5	0.5	0.5	0.5	0.5
Niax A1						0.1	0.1			0.1	0.1	0.1
D 33 LV	0.5	0.3	0.5	0.5	0.5	0.6	0.6	0.5	0.5	0.6	0.6	0.6
Isocyanate A	100	100	114	100	100	100	100	100	100	100	100	100
Isocyanate B	25	25	25	25	30	15	15	10	10	15	10	15
NCO index	100	97	106	77	98	97	97	98	98	97	98	97

Properties	Examples											
	1	2	3	4	5	6	7	8	9	10	11	12
Cells	open*	open	open*	open*	open	open	open	open	open	open	open	open
Recession %	0	0	0	0	1	6	6	6	1	20	10	2
FRD (kg/cm ³)	42	58	47	41		45.8	51.1	54	55			
Foaming												
Cream Time (s)						16	16			69	85	103
End Of Rise (s)						93	97	160	153			
Compression hardness												
CLD 40 % (kPa)	2.3	4.1	2.8	2		2.6	3.2			2.9	2.4	2.3
Hysteresis (%)	18.9	17.1	19.6	19.2		18.5	18.6			10.6	12.2	14.4
Compression set (thick)												
Dry 75 % (%)										6.5	3.3	4
Humid 75 % (%)										1.4	-2.3	-1.7
Resilience (%)	58	62	51	48				62	51	53.6	52.5	47.5
Tear strength												
Max (N/m)										151.8	135.4	156.9
Tensile strength (kPa)										60.3	43	56.7
Elongation (%)										99.9	102.4	126.3

* borderline

CLAIMS

1. A prepolymer process for preparing a high resilience flexible polyurethane foam at an NCO index of 70-120 by reacting :

a) a polyisocyanate composition comprising at least 80% by weight of 4,4'-MDI;

b1) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxy functionality of 2-6, where the EO is present as tipped EO and/or random EO, the total EO content being at least 50 % by weight;

b2) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxy functionality of 2-6, where the EO is present as tipped EO and/or random EO, the total EO content being between 20-50 % by weight, having a primary hydroxy content of at least 50%;

b3) a polyoxyethylene-polyoxypropylene polyol, having an average nominal hydroxyl functionality of 2-6, having a primary hydroxy content of at least 50%, and having an EO content of from 10 to 20 % by weight;

these polyols b1, b2 and b3 being reacted according to the following proportions, based on the combined weights of b1, b2 and b3, b1 : 40-90 wt %, b2 : 5-60 wt %, b3 : 0-20 wt %;

c) water; and

d) additives and auxiliaries known per se;

and where the polyisocyanate prepolymer has an NCO value below 20% by weight.

2. The process according to claim 1, wherein these polyols b1, b2 and b3 are reacted according to the following proportions, based on the combined weights of b1, b2 and b3, b1 : 50-80 wt %, b2 : 10-40 wt %, b3 : 0-10 wt %.

3. The process of claims 1-2, wherein the polyol b2) is of the -PO-PO/EO-EO type.

4. The process of claims 1-2, wherein the polyol b2) is of the -PO/EO-EO type.

5 5. The process of claims 1-2, wherein the polyol b2) is of the -PO-EO type.

6. The process of claims 1-5, wherein the functionality of the polyols b1, b2 and b3 is 2-4.

10 7. The process of claims 1-6, wherein the polyols b1 to b3 further comprise dispersed particles.

15 8. The process of claims 1-7, wherein the NCO value is from 7 to 15% by weight.

20 9. A reaction system comprising A) a polyisocyanate prepolymer having an NCO value of from 7 to 20% by weight, obtained by reacting the polyisocyanate with part of the polyol composition according to claims 1-7, and B) an isocyanate-reactive component comprising the remainder of the polyol composition of claims 1-7 and water.

25 10. The reaction system of claim 9, in which the part of the polyol composition is comprised of the polyol b1).

INTERNATIONAL SEARCH REPORT

Inter. nal Application No
PCT/EP 00/09731

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0 331 941 A (MOBAY) 13 September 1989 (1989-09-13) page 2, line 34 -page 4, line 4; examples ---	1
A	EP 0 296 449 A (BAYER) 28 December 1988 (1988-12-28) page 3, line 8 -page 4, line 5; example 16 -----	1

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/EP 00/09731

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
EP 557792	A	01-09-1993	DE 4205934 A	02-09-1993
			AT 140017 T	15-07-1996
			CA 2090662 A,C	28-08-1993
			DE 59303097 D	08-08-1996
			DK 557792 T	29-07-1996
			ES 2088603 T	16-08-1996
			US 5374667 A	20-12-1994
			US 5534185 A	09-07-1996
WO 9424183	A	27-10-1994	CA 2158648 A	27-10-1994
			CN 1120848 A,B	17-04-1996
			CN 1183422 A	03-06-1998
			EP 0694047 A	31-01-1996
			JP 8511286 T	26-11-1996
			US 5459170 A	17-10-1995
EP 609982	A	10-08-1994	AU 668784 B	16-05-1996
			AU 5310294 A	04-08-1994
			CA 2113946 A	03-08-1994
			CN 1095386 A,B	23-11-1994
			DE 69406319 D	27-11-1997
			DE 69406319 T	19-03-1998
			ES 2108372 T	16-12-1997
			HK 1003835 A	06-11-1998
			JP 6256454 A	13-09-1994
			MX 9400820 A	31-08-1994
			US 5565498 A	15-10-1996
			US 5594097 A	14-01-1997
EP 331941	A	13-09-1989	DE 3806476 A	14-09-1989
			AU 3090989 A	07-09-1989
			CA 1319786 A	29-06-1993
			DE 58904380 D	24-06-1993
			ES 2054895 T	16-08-1994
			JP 1263110 A	19-10-1989
			JP 2587290 B	05-03-1997
			US 5063253 A	05-11-1991
EP 296449	A	28-12-1988	DE 3721058 A	05-01-1989
			AU 604131 B	06-12-1990
			AU 1823888 A	05-01-1989
			CA 1309803 A	03-11-1992
			DE 3862167 D	02-05-1991
			DK 349588 A	27-12-1988
			JP 1022915 A	25-01-1989
			US 4833176 A	23-05-1989

THIS PAGE BLANK (USPTO)